

# ECE 147C

## Solutions, Problem 6.2 (Noisy identification).

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The Simulink block provided corresponds to a discrete-time system with transfer function

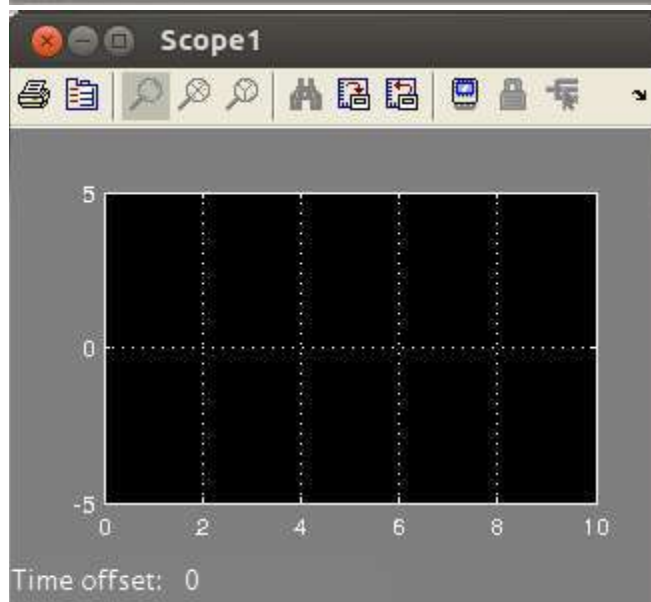
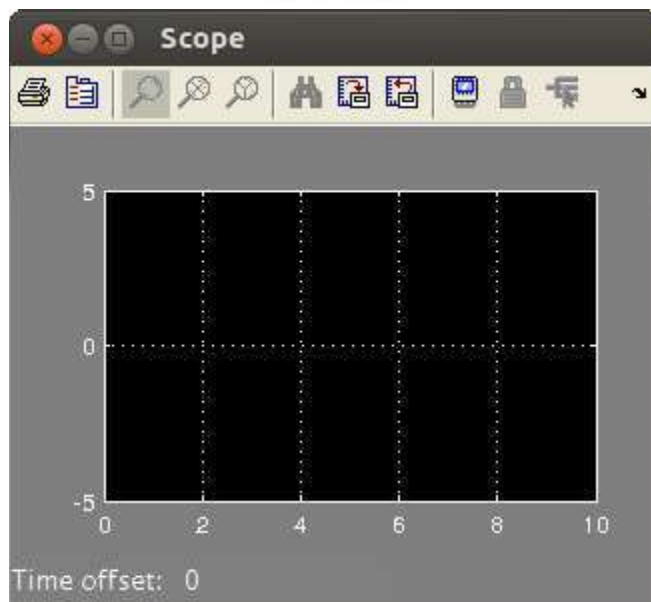
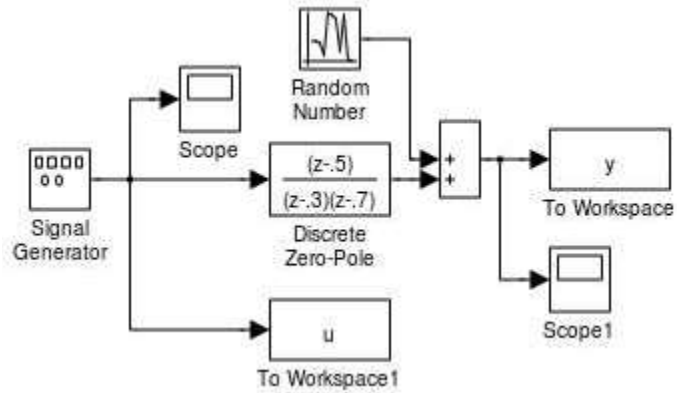
$$H(z) := \frac{\alpha_1 z + \alpha_0}{z^2 + \beta_1 z + \beta_0}$$

```
clc; clear all; close all
```

### Part 1

Use least-squares to estimate the 4 coefficients of the transfer function. Repeat the identification experiment 25 times to obtain 25 estimates of the system's transfer functions.

```
T = 0.01;    % sampling period for the .mdl's disc-time zero-pole block  
[sec/sample]  
N=25;       % # times to run model  
  
open robust_p2_mod
```



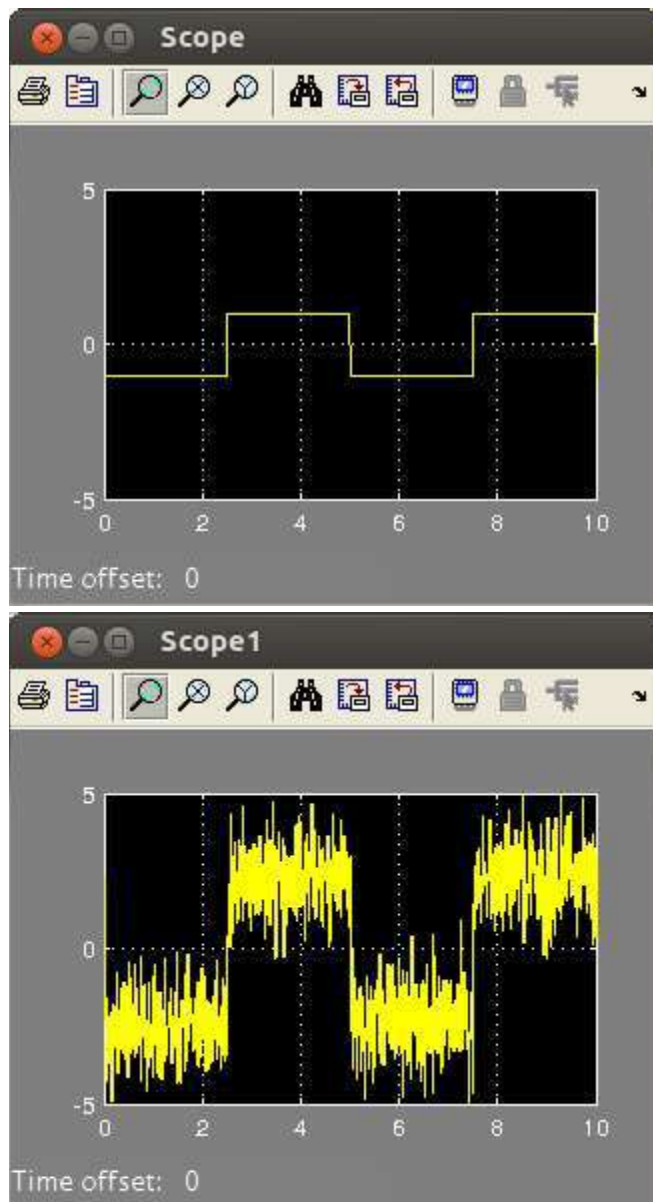
The given  $H$  has order:

```
n=2;  
m=1;
```

Simulate the system 25 times and estimate the TF. Please see the `my_id` function for details about its implementation.

```
% Store identification data here:  
tfs = struct();  
  
for i = 1:N  
    sim('robust_p2_mod',10);  
    [num,den,SSE,MnSV1,MxSV1] = my_id(u,y,2,1);  
    tfs(i).num = num;  
    tfs(i).den = den;  
    tfs(i).SSE = SSE;  
    tfs(i).MnSV1 = MnSV1;  
    tfs(i).MxSV1 = MxSV1;  
end  
  
whos tfs  
  
clearvars -EXCEPT tfs N T
```

| Name | Size | Bytes | Class  | Attributes |
|------|------|-------|--------|------------|
| tfs  | 1x25 | 15920 | struct |            |



## Part 2

Convert the discrete-time transfer functions so obtained to continuous-time using the Tustin transformation.

Hint: Use the MATLAB command `d2c`.

```
for i = 1:N
    num = tfs(i).num;
    den = tfs(i).den;

    P{i} = d2c(tf(num,den,T), 'tustin');
end
```

```
clearvars -EXCEPT P N T
```

### Part 3

Select a nominal model and compute the corresponding additive and multiplicative uncertainty bounds.

Nominal Continuous Plant:

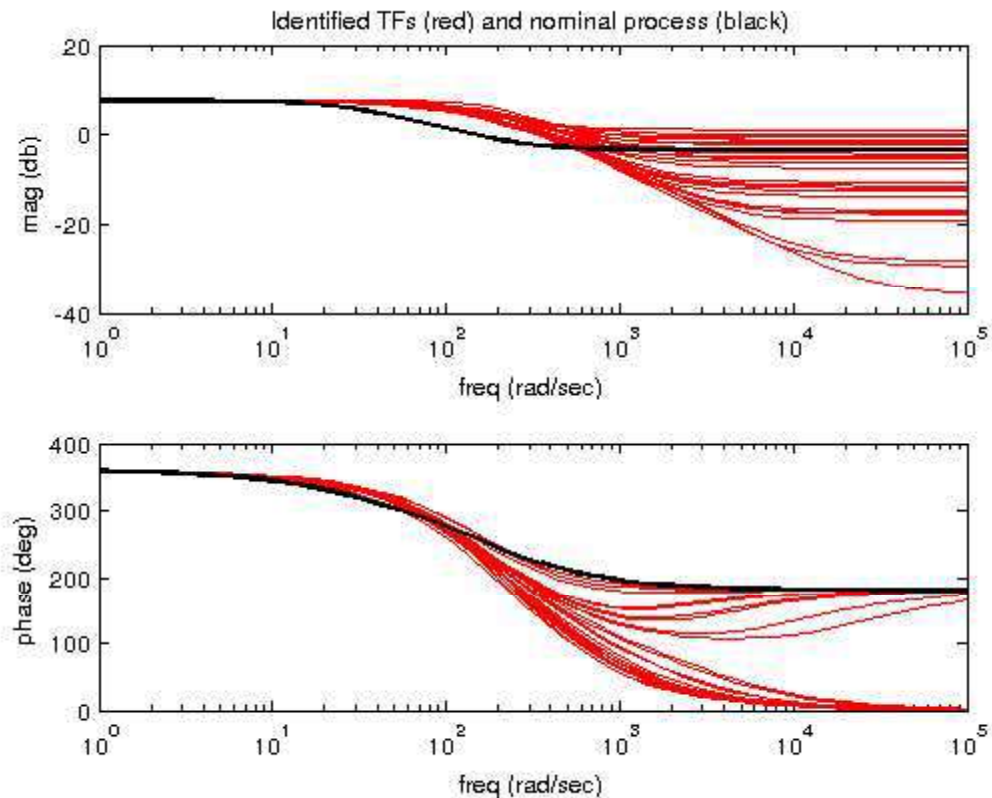
```
P0 = d2c(tf([1 -0.5],[1 -1 0.21]),T),'tustin');
```

Plot to see if it looks representative of the estimated actual plants.

```
figure(1); clf;
w = logspace(0,5);
P{N+1} = P0; % hack
for i=1:N+1
    if i==N+1; sty = {'k-','linewidth',2}; else; sty = {'r-'}; end;

    [mag,phase] = bode(P{i},w);
    mag = squeeze(mag); phase = squeeze(phase);
    magdb = 20*log10(mag);
    figure(1); subplot(2,1,1);
    semilogx(w,magdb,sty{:}); hold on;
    subplot(2,1,2);
    semilogx(w,phase,sty{:}); hold on;
end
subplot(2,1,1); ylabel('mag (db)'); xlabel('freq (rad/sec)')
title('Identified TFs (red) and nominal process (black)')
subplot(2,1,2); ylabel('phase (deg)'); xlabel('freq (rad/sec)')

P = P(1:end-1); % undo hack
clearvars -EXCEPT P0 N P
```



Looks like a pretty good compromise.

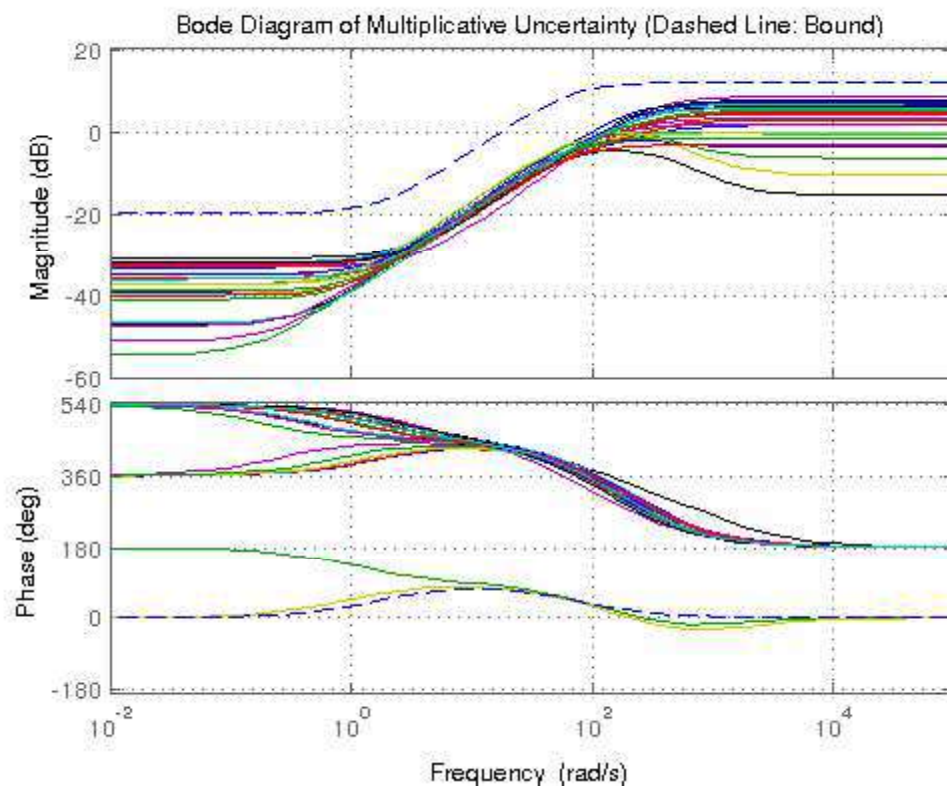
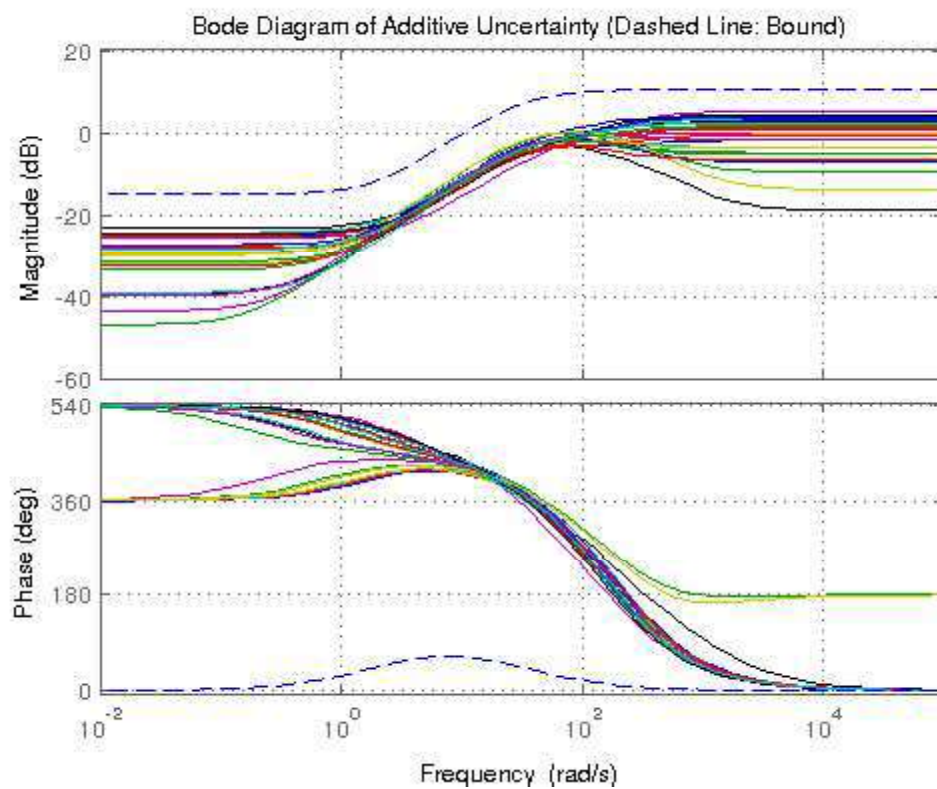
Compute uncertainty.

```
for i = 1:N
    % Additive Uncertainty
    AU{i} = P{i} - P0;

    % Multiplicative Uncertainty
    MU{i} = AU{i} / P0;
end
```

Plot.

```
figure(1); clf; bode(AU{:}); grid on;
title('Bode Diagram of Additive Uncertainty (Dashed Line: Bound)');
la = tf([3.3 6],[1 34]);
hold on; bode(la,'--');
figure(2); bode(MU{:}); grid on;
title('Bode Diagram of Multiplicative Uncertainty (Dashed Line: Bound)');
lm = tf([4 7],[1 70]);
hold on; bode(lm,'--');
```



# ECE 147C

## Solutions, Problem 6.3 (Small gain).

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For the nominal process model and multiplicative uncertainty that you obtained in Exercise 6.2, use the small gain condition to verify if the following controllers achieve stability for all admissible process models:

```
C{1} = tf(0.3,1);  
C{2} = tf(2,[1 0.1]);  
C{3} = tf(20,[1 -30]);  
C{4} = zpk(-1,[-2 -3],5);  
C{5} = zpk(-1,[-0.3 -0.3],2);
```

Justify your answers with appropriate Bode plots.

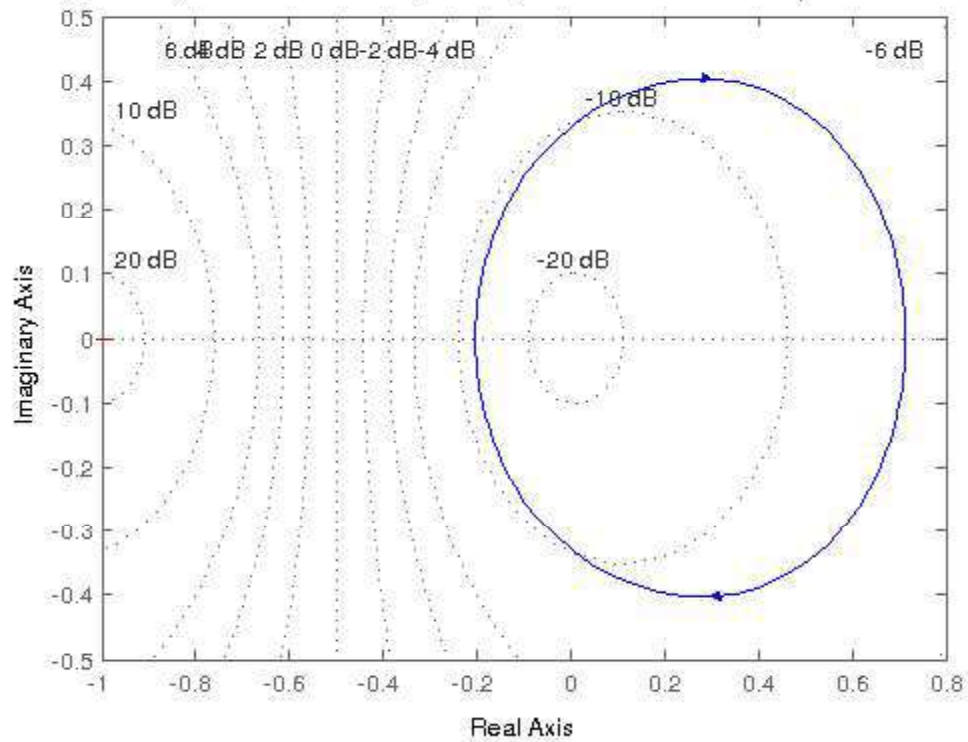
Load the process model and multiplicative uncertainty:

```
load P6 2 results P0 lm C  
Warning: Variable 'C' not found.
```

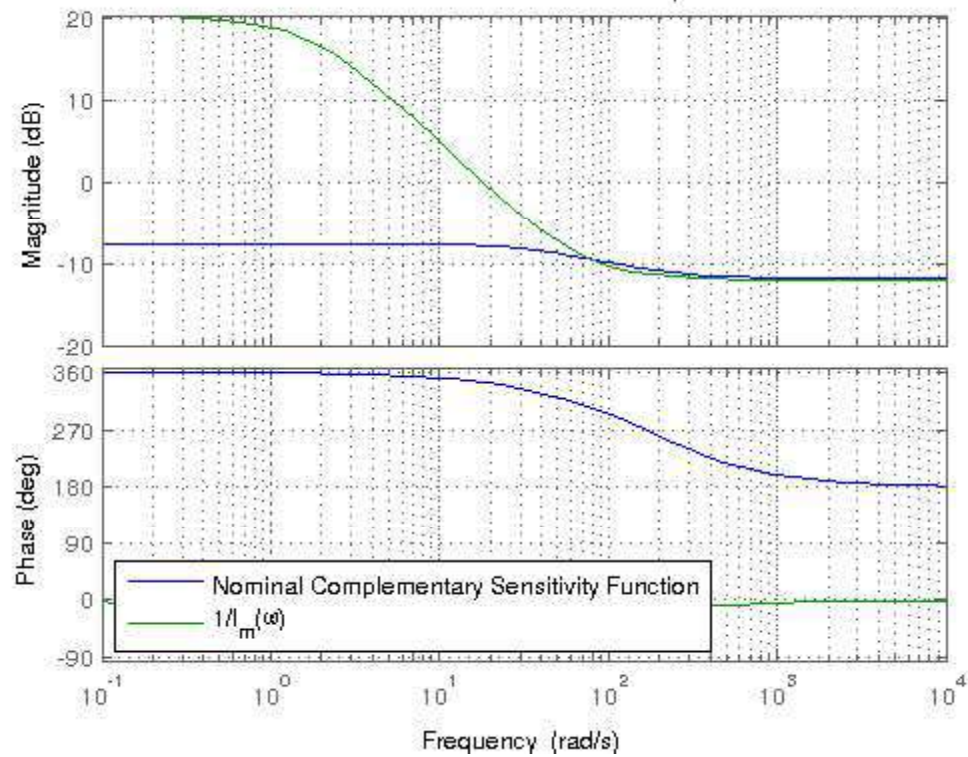
### Controller 1

```
i=1;  
plot_controller
```

Nyquist Diagram of the Nominal Open-Loop Transfer Function with  $C_1$  as the Controller



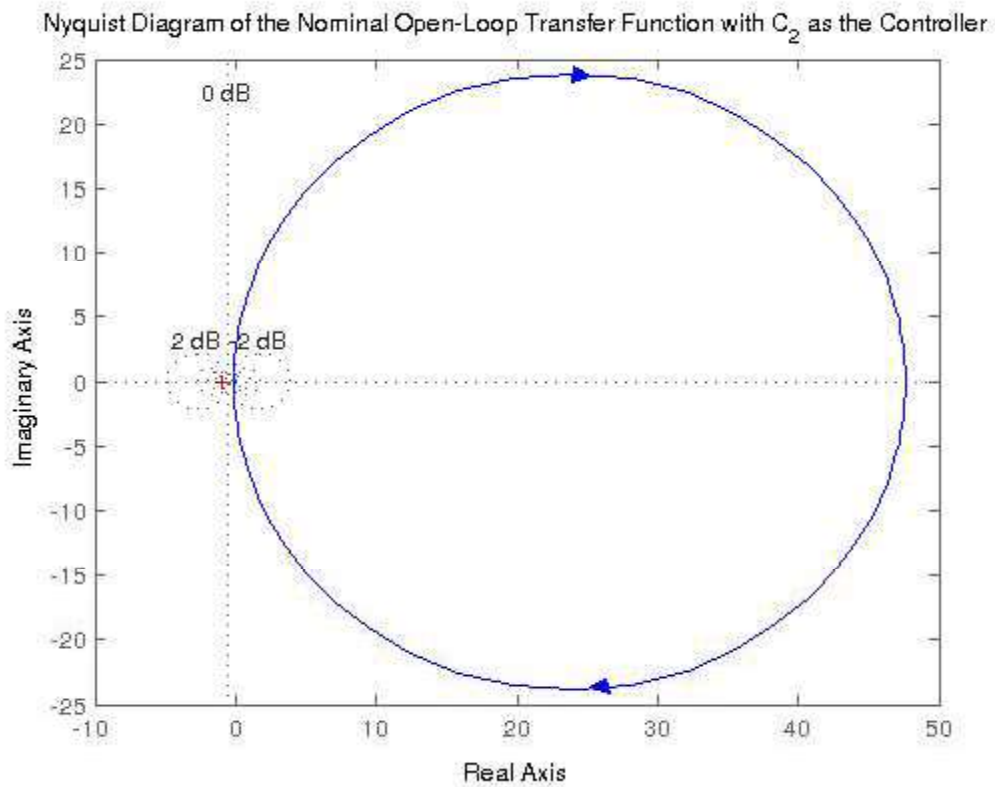
Evaluation of the Small Gain Condition with  $C_1$  as the Controller

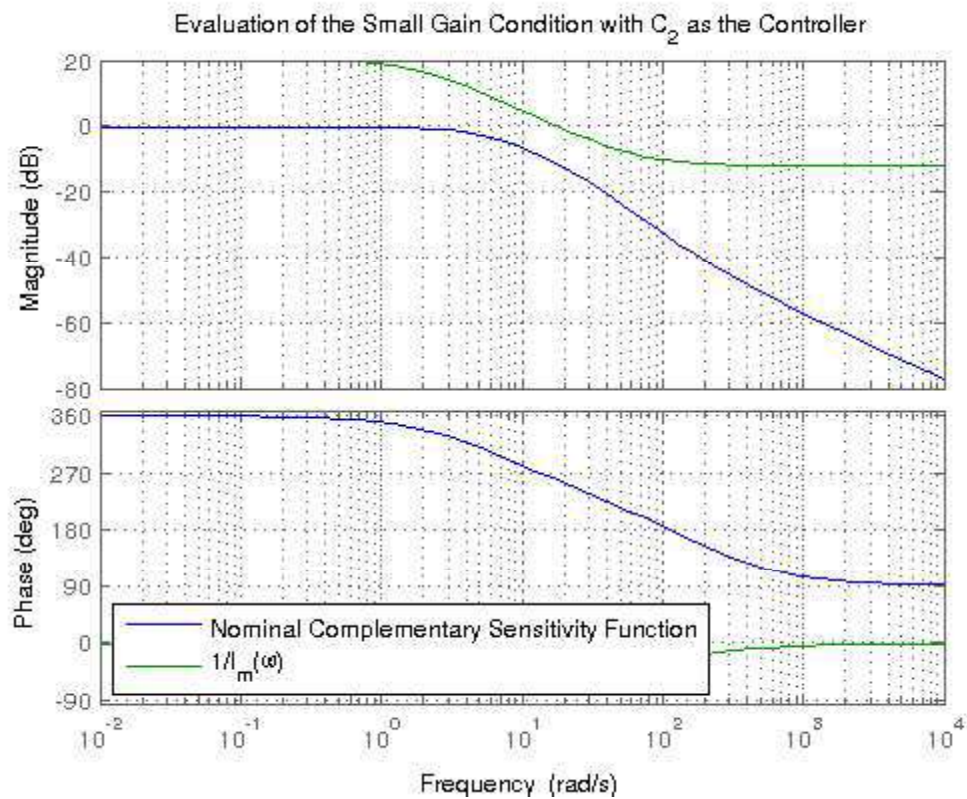


C1 stabilizes the nominal plant, but the small gain condition is not always satisfied.  
Not a Robust Controller.

## Controller 2

```
i=2;  
plot_controller
```



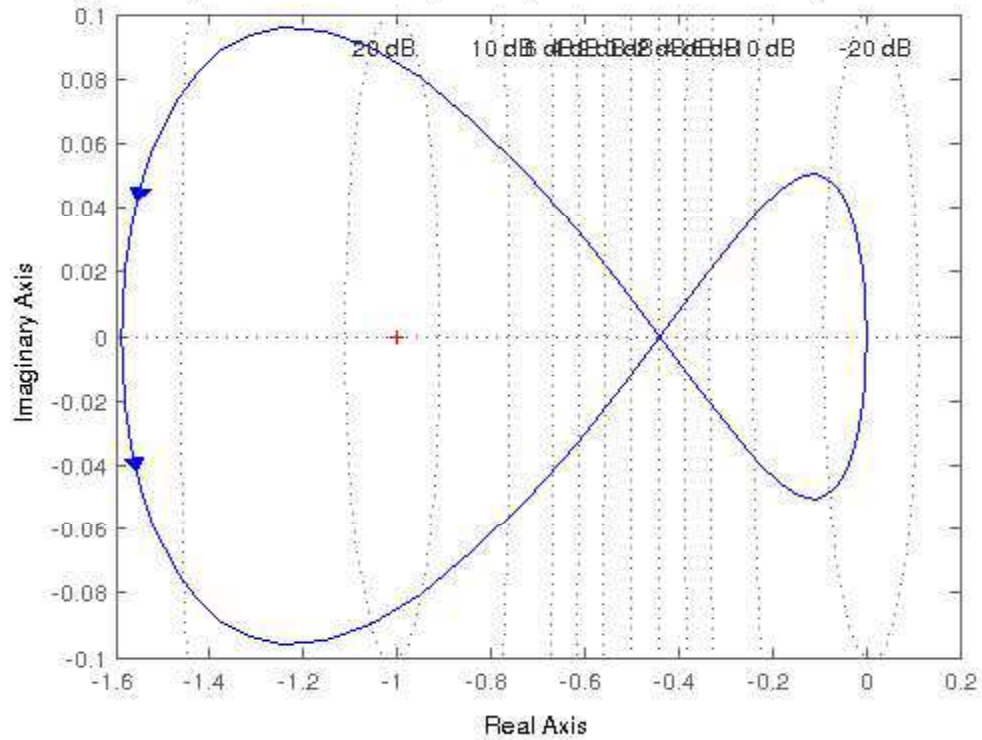


$C_2$  stabilizes the nominal plant and the small gain condition is also satisfied. A Robust Controller.

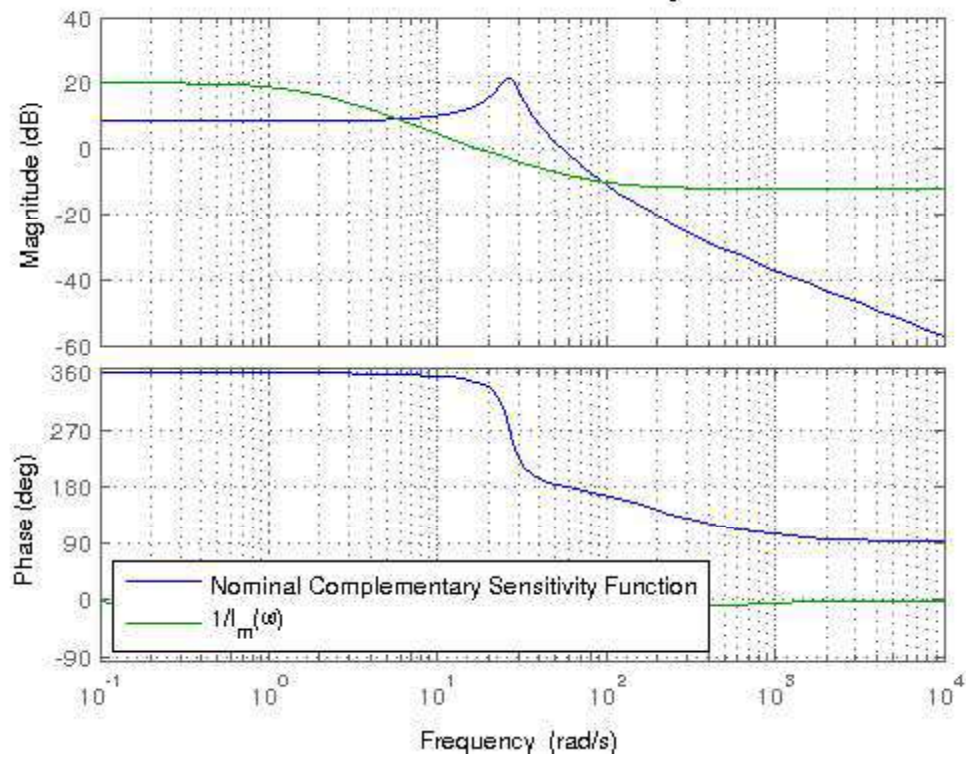
### Controller 3

```
i=3;
plot_controller
```

Nyquist Diagram of the Nominal Open-Loop Transfer Function with  $C_3$  as the Controller



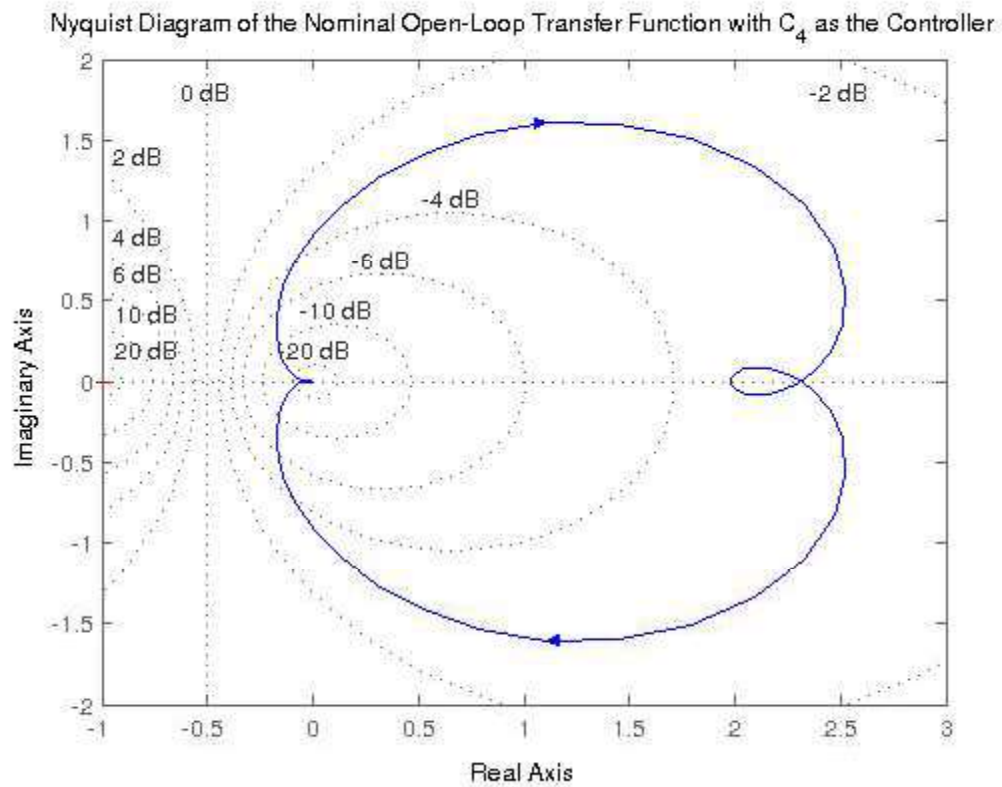
Evaluation of the Small Gain Condition with  $C_3$  as the Controller

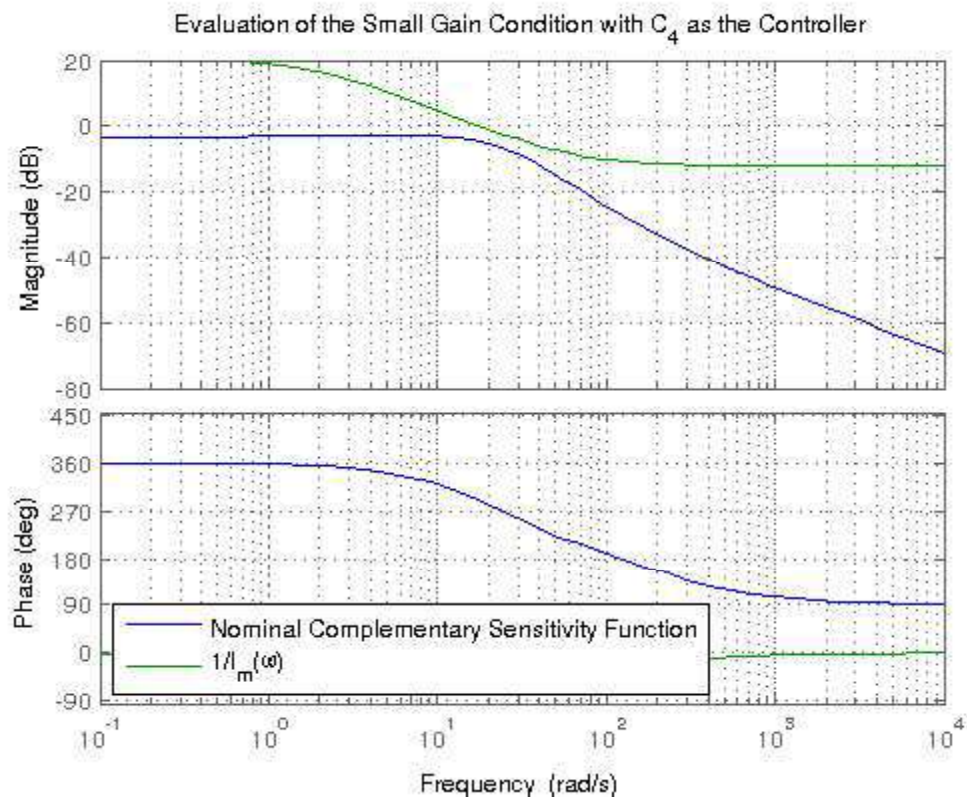


With C3 as the controller, the small gain condition is not always satisfied. Not a Robust Controller

### Controller 4

```
i=4;  
plot_controller
```

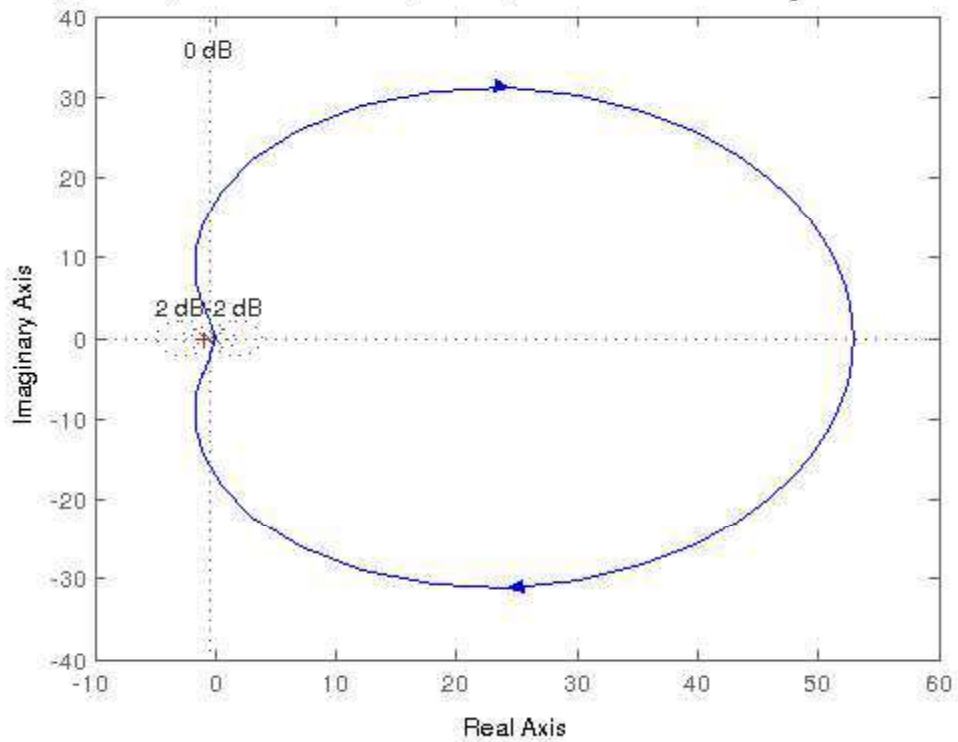




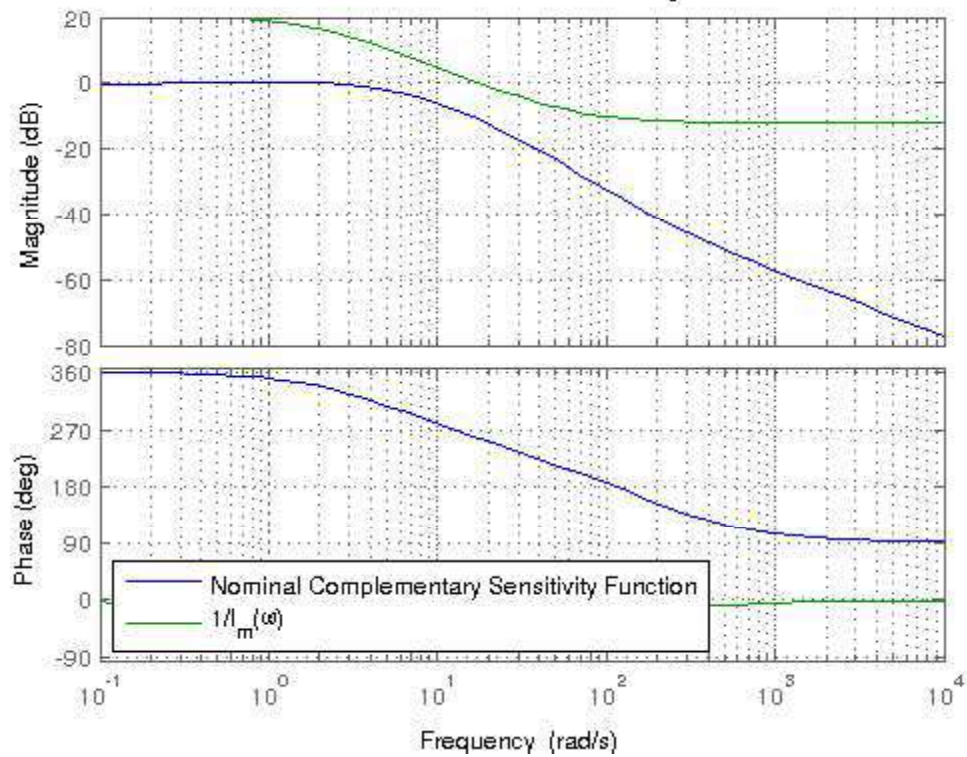
$C_4$  stabilizes the nominal plant and the small gain condition is also satisfied. A Robust Controller.

```
i=5;
plot_controller
```

Nyquist Diagram of the Nominal Open-Loop Transfer Function with  $C_5$  as the Controller



Evaluation of the Small Gain Condition with  $C_5$  as the Controller



C5 stabilizes the nominal plant and the small gain condition is also satisfied. A Robust Controller.